

Add Economizers to Boilers to Recapture Heat from the Flue Exhaust (Arc 2.2421)

(The analysis below was extracted from one of the assessment reports by the Clemson University Industrial Assessment Center (IAC). This is only an example recommendation and hence, not all the background information and sources for numbers are included here.)

<i>Est. Gas Consumption Savings</i>	= 11,157.4 MMBtu/yr
<i>Est. Gas Consumption Cost Savings</i>	= \$47,531 /yr
<i>Est. Implementation Cost</i>	= \$15,500
<i>Simple Payback Period</i>	= 3.9 months

Recommended Action:

It is recommended that an economizer be added to the boiler systems to recapture the heat from the flume exhaust and use it for pre-heating the boiler feed water.

Background:

The plant uses two Clayton Industries Model E504 Standard boilers with 500HP capacity fueled with natural gas. One of the boilers is running throughout the year and the other one is used only for redundancy cases. Economizers are air-to-liquid heat exchangers designed to preheat boiler feed water. They may also be used to heat process of domestic water, or to provide hot liquids for space heating or make-up air heating equipment.

Most economizers have finned tube heat exchangers constructed of stainless steel while the inlet and outlet ducts are carbon steel lined with suitable insulation. Maximum recommended waste gas temperatures for standard units are around 1,800°F.

According to economizer manufacturers, fuel consumption is reduced approximately 1% for each 40°F reduction in flue gas temperature. The higher the flue gas temperature, the greater the potential for energy savings. The following graph shows the effect of pre-heating combustion air on available heat:

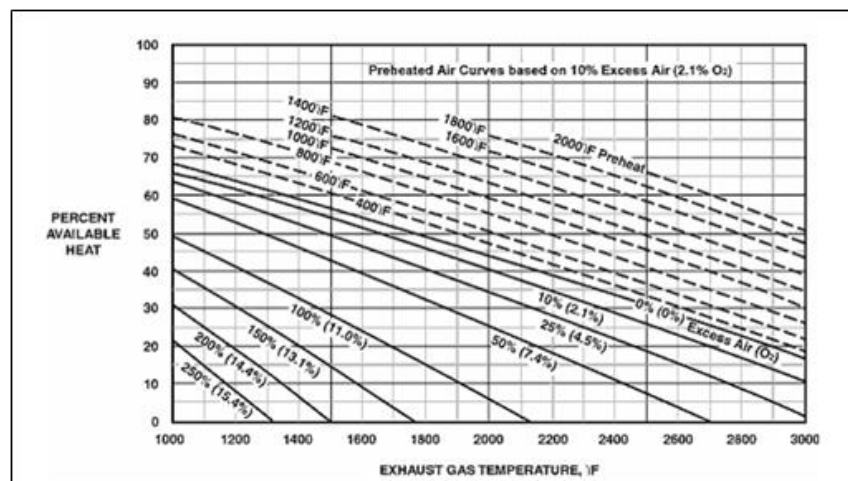


Figure 1. The effect of pre-heating combustion air on available heat.

The average annual natural gas consumption for the plant from years 2015 and 2016 has been 114,226 MMBtu. The average unit cost that the plant is being charged for natural gas is \$4.26/MMBtu.

Anticipated Savings:

The gas-fired combustion efficiency of the boiler was measured at 79.2% using the Bacharach Insight Plus analyzer. According to operations management the steam requirement of the plant is typically around 50% of the boiler capacity. The boiler specifications presented in figure below indicate that the nominal heat input for the installed boiler is about 20.412 MMBtu/h (Figure 2) using natural gas fuel.

MODEL E504	MODEL E504 Standard		MODEL SE504 with Super Economizer		MODEL EG504-FMB with Low NOx Burner			MODEL SEG504-FMB with Low NOx Burner and Super Economizer		
BOILER HORSEPOWER	500		500		500			500		
HEAT INPUT, BTU/hr	20,165,663		19,462,209		NA			NA		
	Oil	20,411,585	19,691,176		20,663,580			19,691,176		
	Gas	16,737,500	16,737,500		16,737,500			16,737,500		
NET HEAT OUTPUT, BTU/hr	17,250		17,250		17,250			17,250		
EQUIVALENT OUTPUT (from and at 212°F feedwater and 0 PSIG steam)	65 - 500 PSIG		65 - 500 PSIG		65 - 500 PSIG			65 - 500 PSIG		
DESIGN PRESSURE (see note 1)	60 - 450 PSIG		60 - 450 PSIG		60 - 450 PSIG			60 - 450 PSIG		
STEAM OPERATING PRESSURE (determined by design pressure)	143.4 gph		138.4 gph		N/A			N/A		
OIL CONSUMPTION at maximum steam output (see note 2)	20,412 cfh		19,691 cfh		20,664 cfh			19,691 cfh		
GAS CONSUMPTION at maximum steam output (see note 3)	5 to 1 Turndown		5 to 1 Turndown		4 to 1 Turndown			4 to 1 Turndown		
BURNER CONTROLS modulating	83%		86%		NA			NA		
EFFICIENCY oil-fired efficiency %	82%		85%		81%			85%		
gas-fired efficiency %	Blower Pump		Blower Pump		Blower Pump Cooling			Blower Pump Cooling		
ELECTRIC MOTORS, HP (see note 4)	25 20		25 20		30 20 7.5			30 20 7.5		
design pressure 15-300 psig	25 30		25 30		30 30 7.5			30 30 7.5		
design pressure 301-500 psig	74		74		92			92		
ELECTRIC FLA, based on 460 V (see note 5)	85		85		107			107		
design pressure 15-300 psig	5 to 10 psig		5 to 10 psig		5 to 10 psig			5 to 10 psig		
design pressure 301-500 psig	30 scfm		30 scfm		NA			NA		
GAS SUPPLY PRESSURE REQUIRED	70 psig		70 psig		NA			NA		
ATOMIZING AIR REQUIRED (see note 6)	N/A		N/A		5 scfm @ 3 to 150 psig			5 scfm @ 3 to 150 psig		
Capacity	2,650 gph		2,650 gph		2,650 gph			2,650 gph		
Minimum pressure	912 sq.ft.		1,207 sq.ft.		912 sq.ft.			1,207 sq.ft.		
AIR SUPPLY REQUIRED (FMB -see note 7)	32 in.		32 in.		32 in.			32 in.		
WATER SUPPLY REQUIRED	133 in.		133 in.		156 in.			156 in.		
HEATING SURFACE	131 in.		131 in.		142 in.			142 in.		
EXHAUST STACK CORRECTION, o.d.	131 in.		157 in.		135 in.			161 in.		
APPROXIMATE OVERALL DIMENSIONS	17,408 lbs		20,400 lbs		17,708 lbs			20,700 lbs		
length	14,790 lbs		17,190 lbs		15,090 lbs			17,490 lbs		
width	2,000 lbs		2,000 lbs		2,000 lbs			2,000 lbs		
height										
WEIGHT										
installed - wet										
shipping										
FW pump skid										

1) Design pressures are available up to 3000 psig. Consult factory for details.
2) Based on No. 2 fuel oil with a High Heat Value (HHV) of 140,600 BTU/Gal.
3) Based on Natural Gas with a High Heat Value (HHV) of 1,000 BTU/ft.³
4) Oil fired units also use a separate motor driven fuel oil pump - 3/4 HP
5) Continuous running. For 575 V multiply by 0.8; for 380 V multiply by 1.1; for 230 V multiply by 2.0; for 208 V multiply by 2.2.
6) Atomizing air required for oil burner.
7) Compressed air required for FMB.
The description and specifications shown were in effect at the time this publication was approved for printing. Clayton Industries, whose policy is one of continuous improvement, reserves the right to discontinue models, or change specifications or design, without notice.

Figure 2. Boiler specifications for Model E504 Standard

Therefore, the annual estimated energy consumption of the boiler, *EEC*, can be determined as follows:

$$EEC = \text{Heat input (MMBtu/h)} \times \text{Steam load (\%)} \times \text{Operational hours}$$

$$EEC = 20.412 \text{ MMBtu/h} \times 50\% \times 8760\text{h} = 89,402.7 \text{ MMBtu}$$

A high quality recuperator could recover up to 60% of this waste heat. Accordingly, the potential energy savings from the installation of a recuperator on the process boiler, AES, can be determined as:

$$AES = EEC \times (1 - \text{Eff}_1) \times RC$$

where RC is the percent of energy recoverable by recuperator, so

$$AES = 89,4012.7 \times (1 - 0.792) \times 0.6 = 11,157.4 \text{ MMBtu}$$

Finally, the estimated annual energy cost saving, $AECS$, can be determined based on the unit energy consumption charge for natural gas:

$$AECS = AES \times (\$4.26/\text{MMBtu})$$

$$AECS = 11,157.4 \times (\$4.26/\text{MMBtu}) = \$47,531$$

Implementation Cost:

Many boiler companies sell off-the shelf boiler recuperators of various sizes and efficiencies. The cost of a recuperator capable of handling the exhaust flow rate of the boiler as well as having efficiency greater than 70% would be about \$10,000 and the anticipated installations costs would run to about \$5,500. Therefore, the implementation cost, IC , would be approximately around \$15,500.

$$\text{Implementation Cost (IC)} = \$15,500$$

Simple Payback Period:

The *simple payback period*, SPP , is the time required to pass before the estimated total cost savings equal the estimated implementation cost, and is calculated by:

$$SPP = \frac{IC}{AECS} \times 12 \text{ months/year}$$

$$SPP = \frac{15,500}{47,531} \times 12 \text{ months/year}$$

$$SPP = 3.9 \text{ months}$$