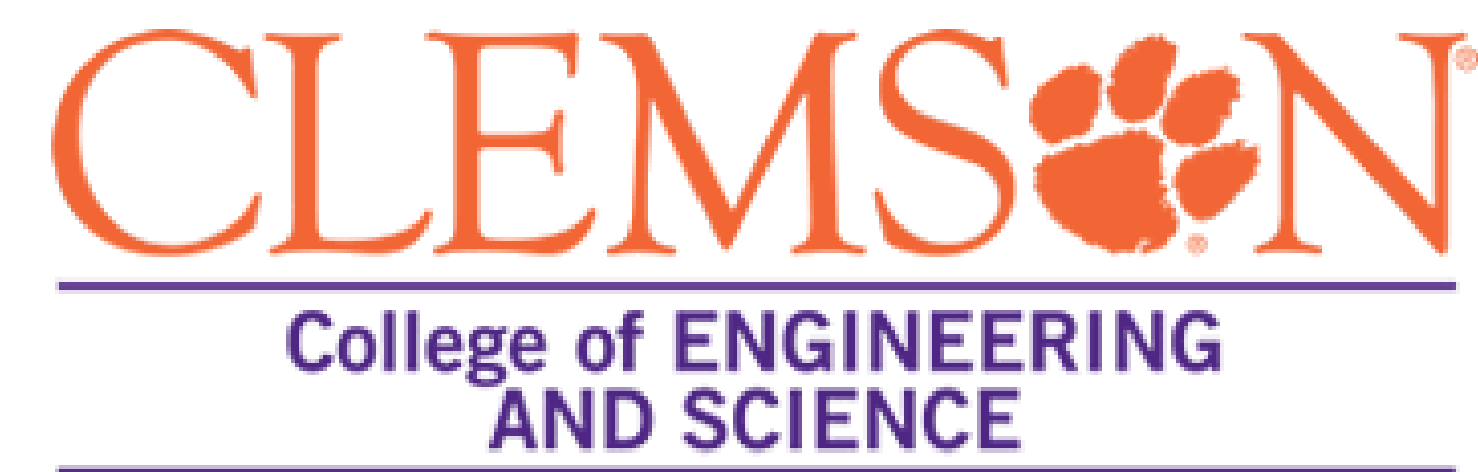


# Concentration polarization modeling for high-pressure membranes with engineered surface features

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## 1: Motivation & Objectives

### Motivation

- Concentration polarization reduced performance of membranes in terms of flux and water quality.
- Fouling is more problematic when concentration polarization is high.

### Objectives

- Develop a computational framework to predict concentration polarization of patterned membranes.
- Evaluate the effect of hydrodynamics on concentration profiles.
- Explore the performance of different membrane patterns.

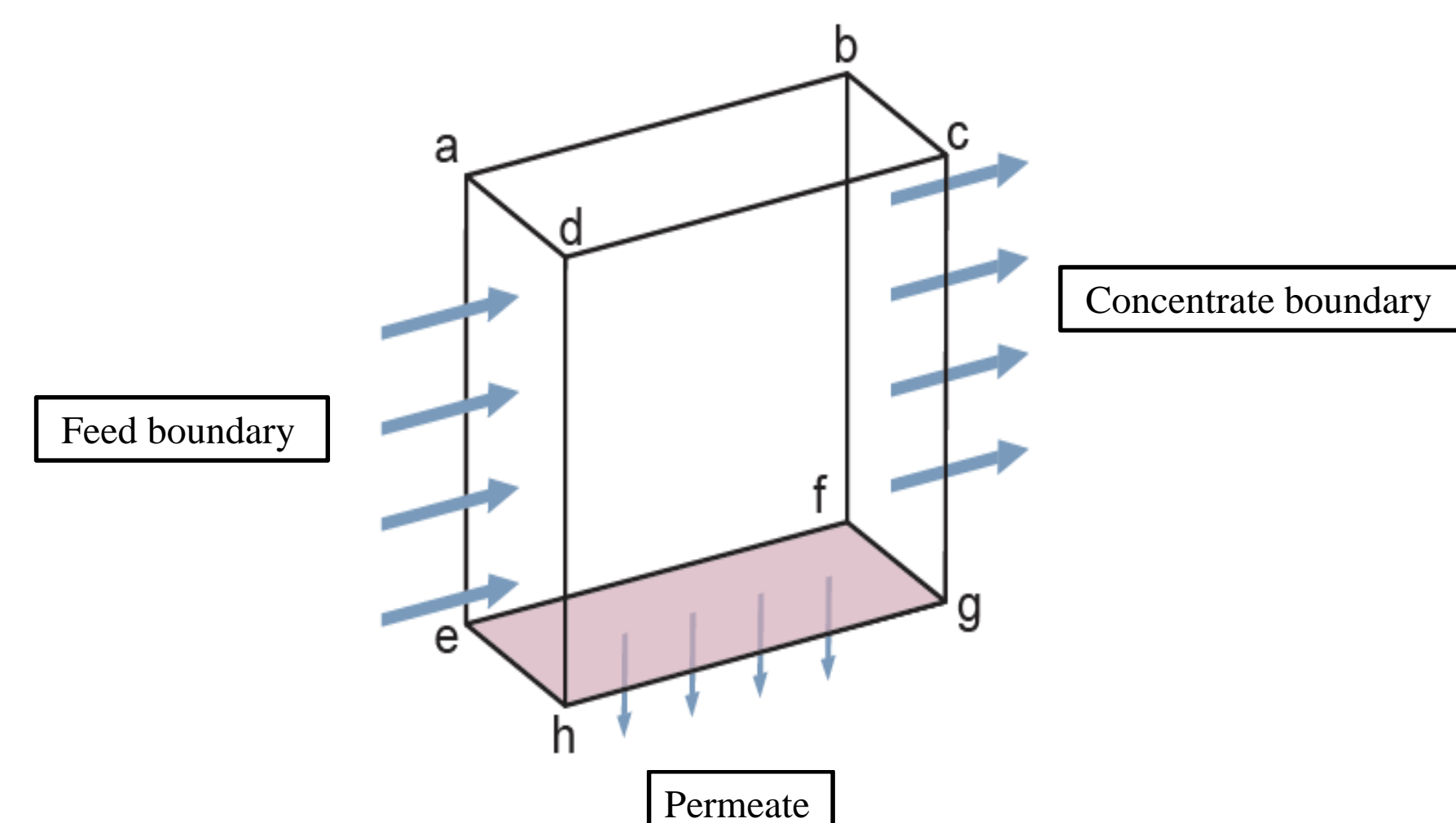
## 2: Model Introduction

### Introduction

- Computational fluid dynamics (CFD) uses numerical analysis to solve and analyze fluid flow problems.
- Models were built with COMSOL Multiphysics (version 5.3).

### Geometry

- Block: width 4.096 mm, depth 2.048 mm, height 8 mm.
- Eight geometry types: elementary shapes including line and grooves, pillars, chords, and pyramids. Mesh: boundary layer along the membrane surface due to drastic gradient changes.
- A pattern size of 512 μm was studied first, and then four smaller sizes were studied: 2 μm, 8 μm, 32 μm, and 128 μm. Velocity was normalized in different geometries based on a total channel height of 16 mm.



(Wall abcd: moving wall. Wall abfe and wall dcgh: periodic boundaries. Membranes are located at efg. Inlet concentration: 0.025 M.)

## 3: Theoretical Description

### Key Governing Equations

- Navier-Stokes  

$$\rho(\nabla \cdot \mathbf{u})\mathbf{u} = -\nabla P + \frac{\mu}{2} \nabla \cdot (\nabla \mathbf{u} + \nabla \mathbf{u}^T)$$
- Conservation of momentum  

$$\nabla \cdot \mathbf{u} = 0$$
- Convective diffusion  

$$\mathbf{u} \nabla c = D_c \nabla^2 c$$

### Key Boundary Conditions

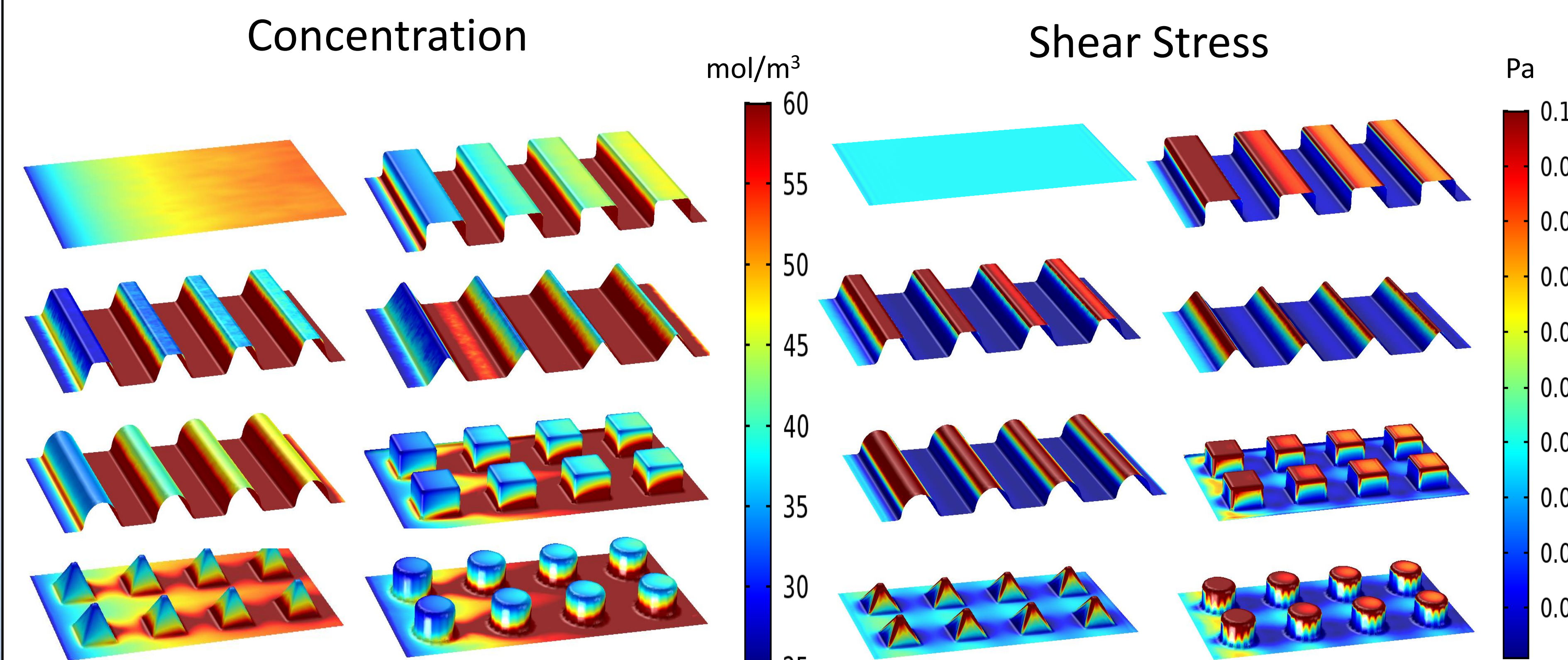
- Permeate flux  

$$u_m = A(\Delta p - a_{osm} c_w)$$
- Inlet velocity  
 (Adjusted based on  $v=0.1$  m/s in a 16 mm channel)
- Outlet pressure  

$$p_{out} = 400 \text{ psi}$$

## 3: Results & Discussion

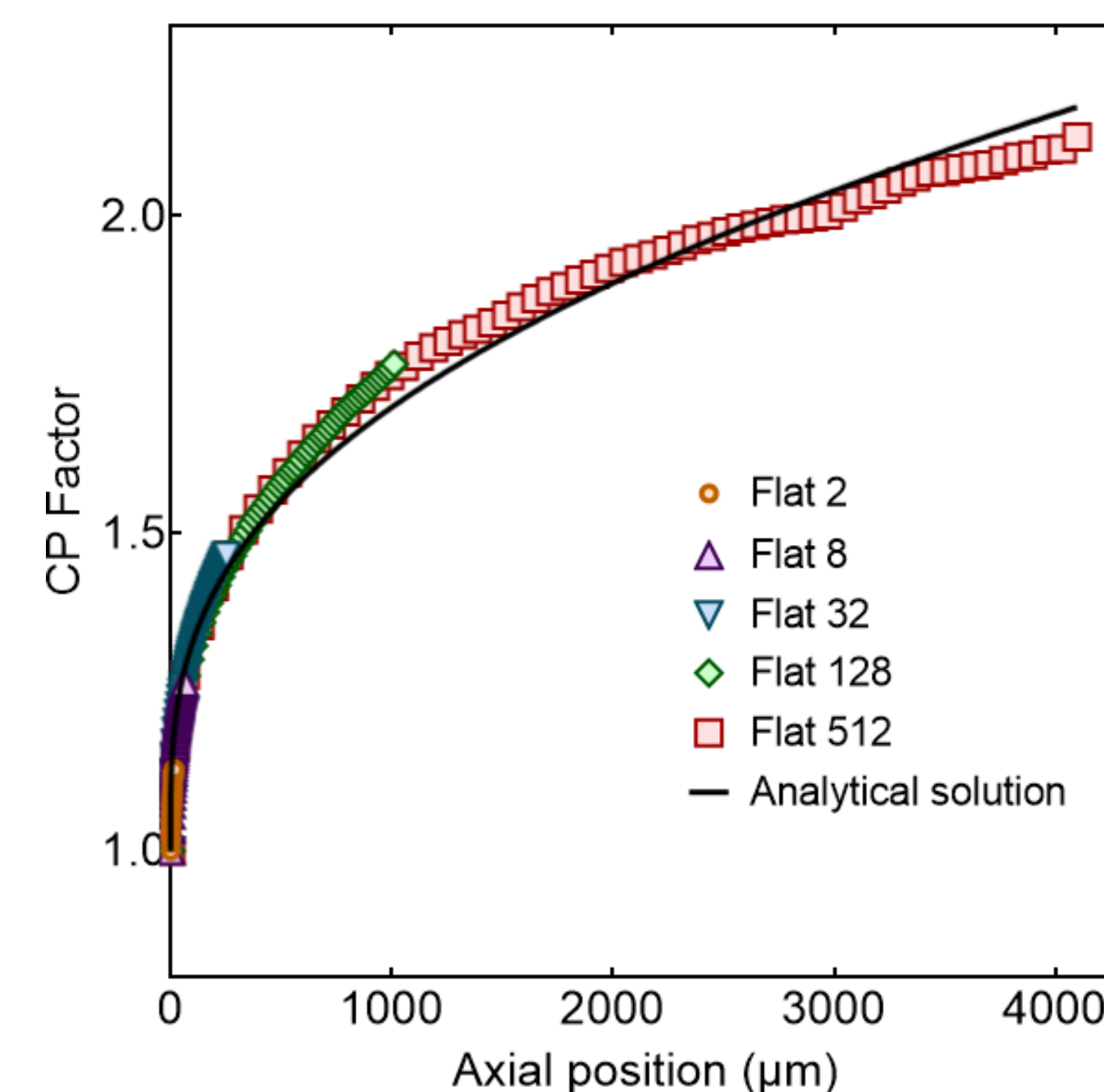
### CONCENTRATION AND SHEAR PROFILES



### ANALYTICAL VS. NUMERICAL SOLUTIONS

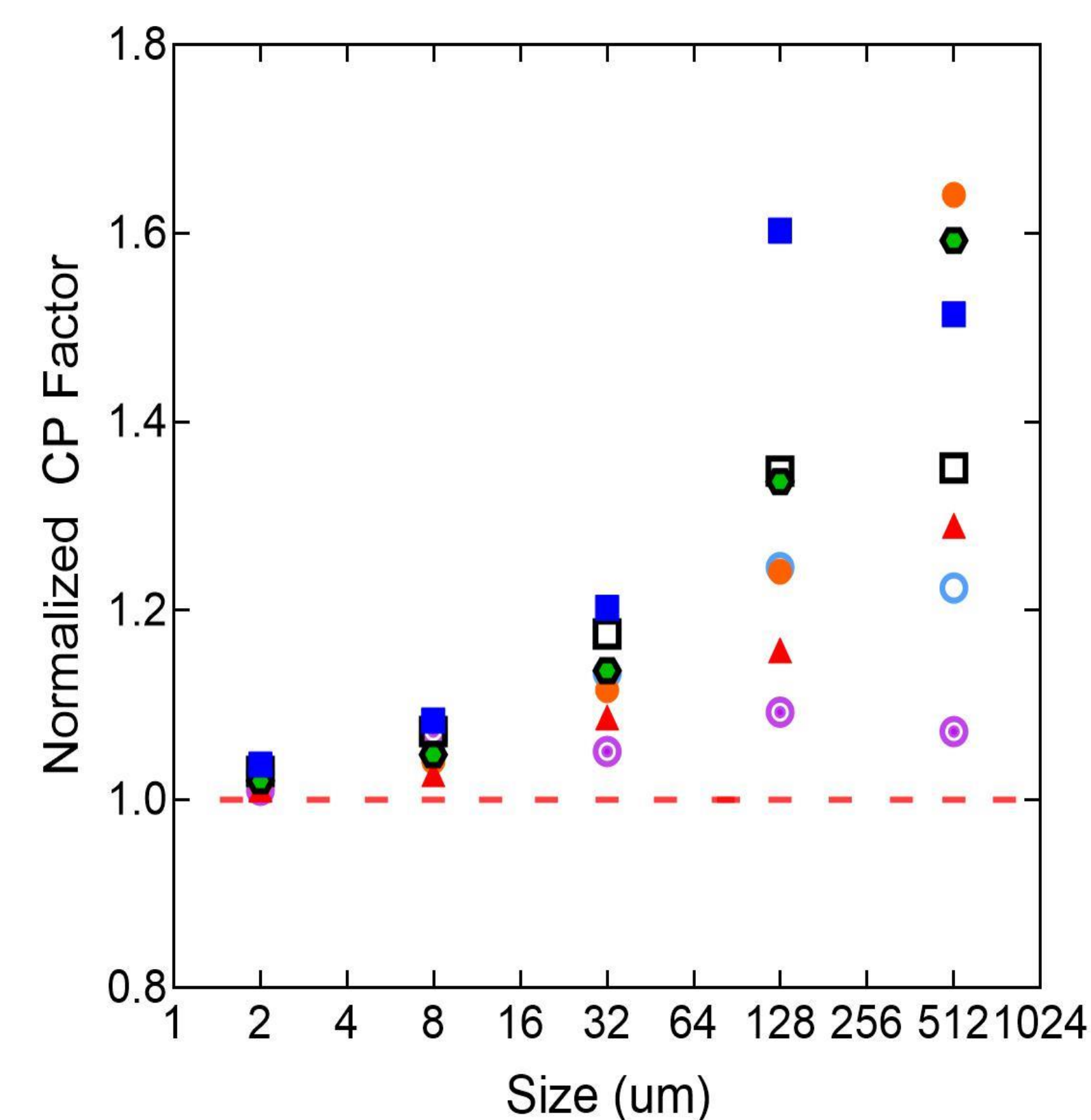
$$Sh = 1.85 \left( Re \cdot Sc \cdot \frac{d_h}{L} \right)^{0.275}$$

$$k = \frac{Sh \cdot d}{d_h} \quad \frac{c_m}{c_b} = \exp\left(\frac{J}{k}\right)$$



### CP RESULTS

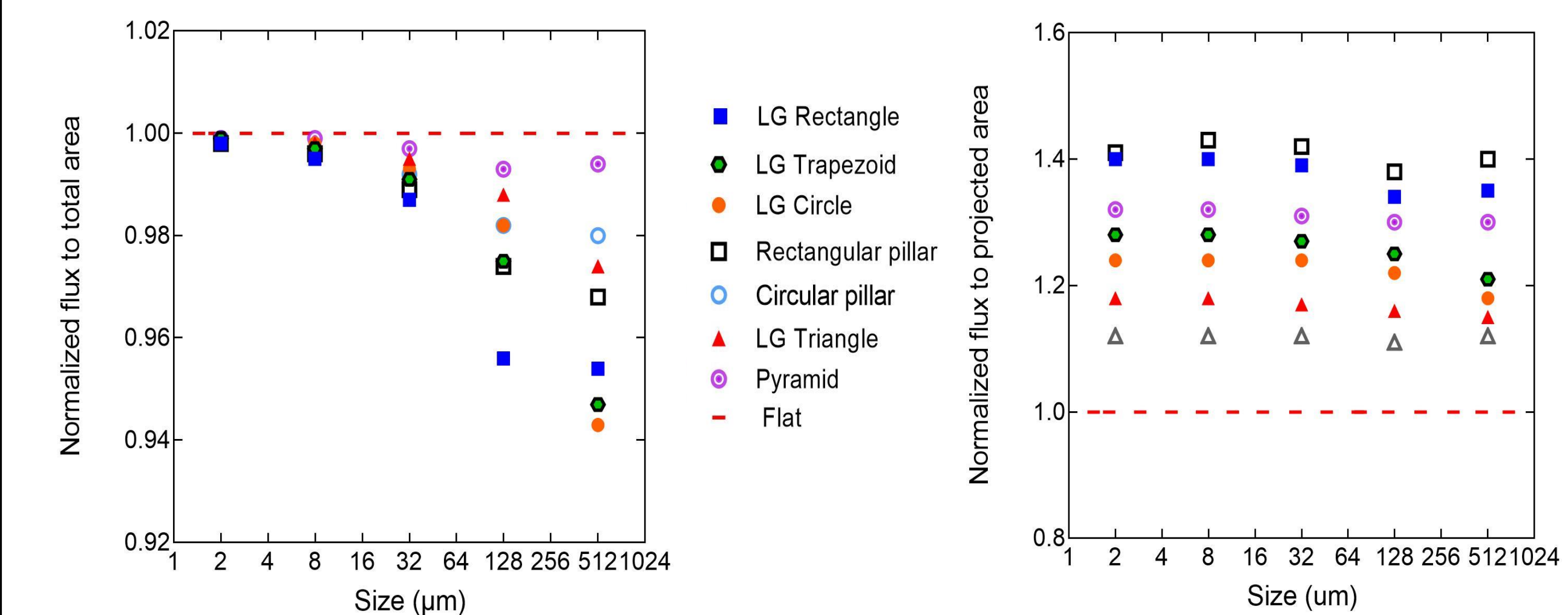
- LG Rectangle
- Rectangular pillar
- LG Trapezoid
- Circular pillar
- LG Circle
- ▲ LG Triangle
- Pyramid
- Flat



## 3: Results & Discussion

### PERMEATE FLUX VS PATTERN SIZES

Feature Length (μm)	Feature Height (=0.5·Length) (μm)	Between-Feature Distance (=Length) (μm)	Fillet (=0.2·Height) (μm)
2 μm	1 μm	2 μm	0.2 μm
8 μm	4 μm	8 μm	0.8 μm
32 μm	16 μm	32 μm	3.2 μm
128 μm	64 μm	128 μm	12.8 μm
512 μm	256 μm	512 μm	51.2 μm



## 4: Conclusions and Looking Forward

- Analytical solutions were used to validate modeling results among all the flat membranes.
- Seven membranes with different surface features were scrutinized and compared with flat membranes. None of the patterns reduced CP.
- Patterns created higher surface areas compared to a flat membrane, leading to a higher nominal flux through the membrane surface in the models.
- The fouling mitigation seen in experiments with nanoscale patterns is likely due to other factors.
- Future studies will incorporate adsorptive fouling.

## 5: Acknowledgements

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- Computational resources provided by the Palmetto Cluster at Clemson University.

## 6: Selected References

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