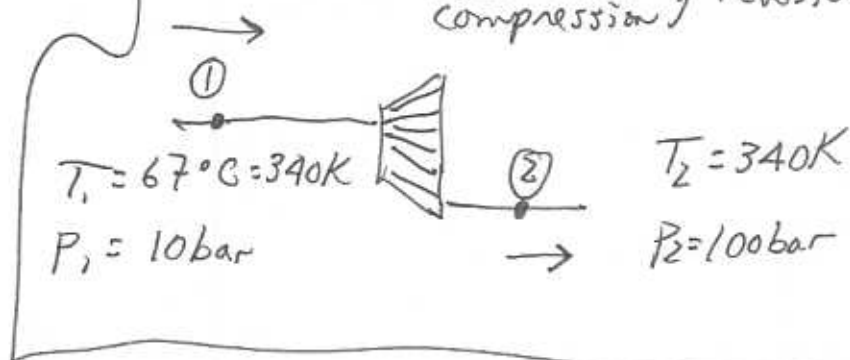


11.84

Ethylene. $\Delta KE = \Delta PE = 0$
S.S.isothermal; reversible
compression; reversible

$$\frac{\dot{W}}{\dot{m}} = ? \quad \frac{\dot{Q}}{\dot{m}} = ?$$

Entropy Balance

$$\frac{dS}{dt} = \sum_j \frac{\dot{Q}_j}{T_j} + \sum_i \dot{m}_i s_i - \sum_e \dot{m}_e s_e + \dot{S}_{c.v.}$$

reversible

S.S.

$$\hookrightarrow \frac{\dot{Q}}{\dot{m}} = T(s_2 - s_1)$$

C.O.E. $\frac{dE}{dt} = \dot{Q} - \dot{W} + \sum_i \dot{m}_i (h_i + \frac{V_i^2}{2} + g z_i) - \sum_e \dot{m}_e (h_e + \frac{V_e^2}{2} + g z_e)$

$$\frac{\dot{W}}{\dot{m}} = \frac{\dot{Q}}{\dot{m}} + (h_1 - h_2)$$

So what we need is Δs and Δh

$$\bar{A}_2 - \bar{A}_1 = (\bar{A}_2^* - \bar{A}_1^*) - \bar{R} \left[\left(\frac{\bar{A}^* - \bar{A}}{\bar{R}} \right)_2 - \left(\frac{\bar{A}^* - \bar{A}}{\bar{R}} \right)_1 \right]$$

$$= (\bar{A}^*(T_2) - \bar{A}^*(T_1)) - R \ln\left(\frac{P_2}{P_1}\right)$$

Ethylene MW = 28.05 kg/kmol $T_c = 283K$ $P_c = 51.2 \text{ bar}$

$$T_R = 1.20$$

$$P_{R1} = 0.195$$

$$P_{R2} = 1.95$$

From Fig A-5

$$\left(\frac{\bar{A}^* - \bar{A}}{\bar{R}} \right)_1 = 0.1$$

$$\left(\frac{\bar{A}^* - \bar{A}}{\bar{R}} \right)_2 = 1.25$$

11.84 (continued)

$$\bar{A}_2 - \bar{A}_1 = \bar{A}^{\circ}(T_2) - \bar{A}^{\circ}(T_1) - \bar{R} \ln\left(\frac{P_2}{P_1}\right) - \bar{R} \left[\left(\frac{\bar{h}^* - \bar{A}}{\bar{R}} \right)_2 - \left(\frac{\bar{h}^* - \bar{A}}{\bar{R}} \right)_1 \right]$$

$$\bar{A}_2 - \bar{A}_1 = - \left(8.314 \frac{\text{kJ}}{\text{kmole} \cdot \text{K}} \right) \ln\left(\frac{100 \text{ bar}}{10 \text{ bar}}\right) - \left(8.314 \frac{\text{kJ}}{\text{kmole} \cdot \text{K}} \right) [1.25 - 0.1]$$

$$\bar{A}_2 - \bar{A}_1 = -28.70 \frac{\text{kJ}}{\text{kmole} \cdot \text{K}}$$

$$\Delta_2 - \Delta_1 = -1.02 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$\therefore \frac{\dot{Q}}{\dot{m}} = (340 \text{ K}) \left(-1.02 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right)$$

$$\boxed{\frac{\dot{Q}}{\dot{m}} = -348 \text{ kJ/kg}}$$

$$\bar{h}_2 - \bar{h}_1 = \bar{h}_2^* - \bar{h}_1^* - \bar{R} T_c \left[\left(\frac{\bar{h}^* - \bar{h}}{\bar{R} T_c} \right)_2 - \left(\frac{\bar{h}^* - \bar{h}}{\bar{R} T_c} \right)_1 \right]$$

0 for an ideal gas when $\Delta T = 0$

From Fig. A-4

$$\left(\frac{\bar{h}^* - \bar{h}}{\bar{R} T_c} \right)_1 = 0.1 \quad \left(\frac{\bar{h}^* - \bar{h}}{\bar{R} T_c} \right)_2 = 1.9$$

$$\bar{h}_2 - \bar{h}_1 = \left(-8.314 \frac{\text{kJ}}{\text{kmole} \cdot \text{K}} \right) (293 \text{ K}) [1.9 - 0.1] = -4235.2 \frac{\text{kJ}}{\text{kmole}}$$

$$h_2 - h_1 = -151 \text{ kJ/kg} \Rightarrow h_1 - h_2 = 151 \text{ kJ/kg}$$

$$\therefore \boxed{\frac{\dot{W}}{\dot{m}} = -197 \text{ kJ/kg}}$$